

MULTI-SCALE UNCERTAINTY ANALYSIS

A tool to systematically consider variability in
lignocellulosic bioethanol processes



Bioethanol in a circular economy



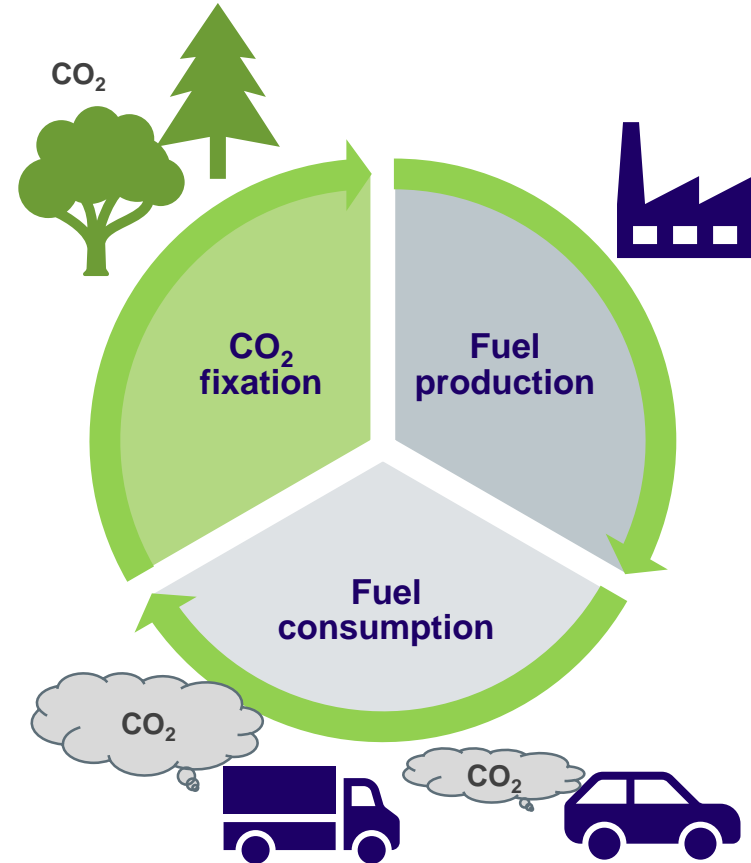
Usage of **fossil fuels** steadily increasing



ca. 50% is used for transportation



Bioethanol sustainable alternative to fossil fuels



Variability in the bioethanol process

Raw materials



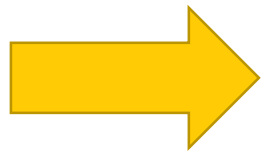
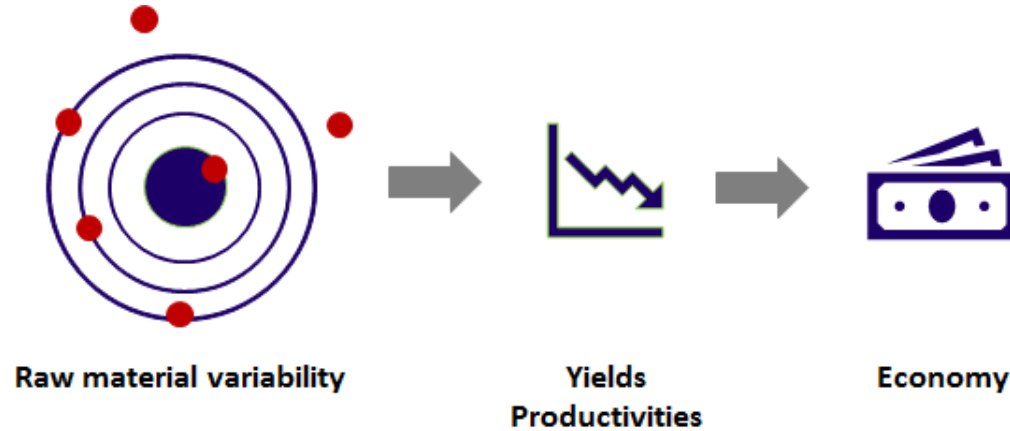
- 🎯 **Location**
- 🎯 **Harvest time**
- 🎯 **Composition of biomass**
- 🎯 **Storage**

Measurement and control



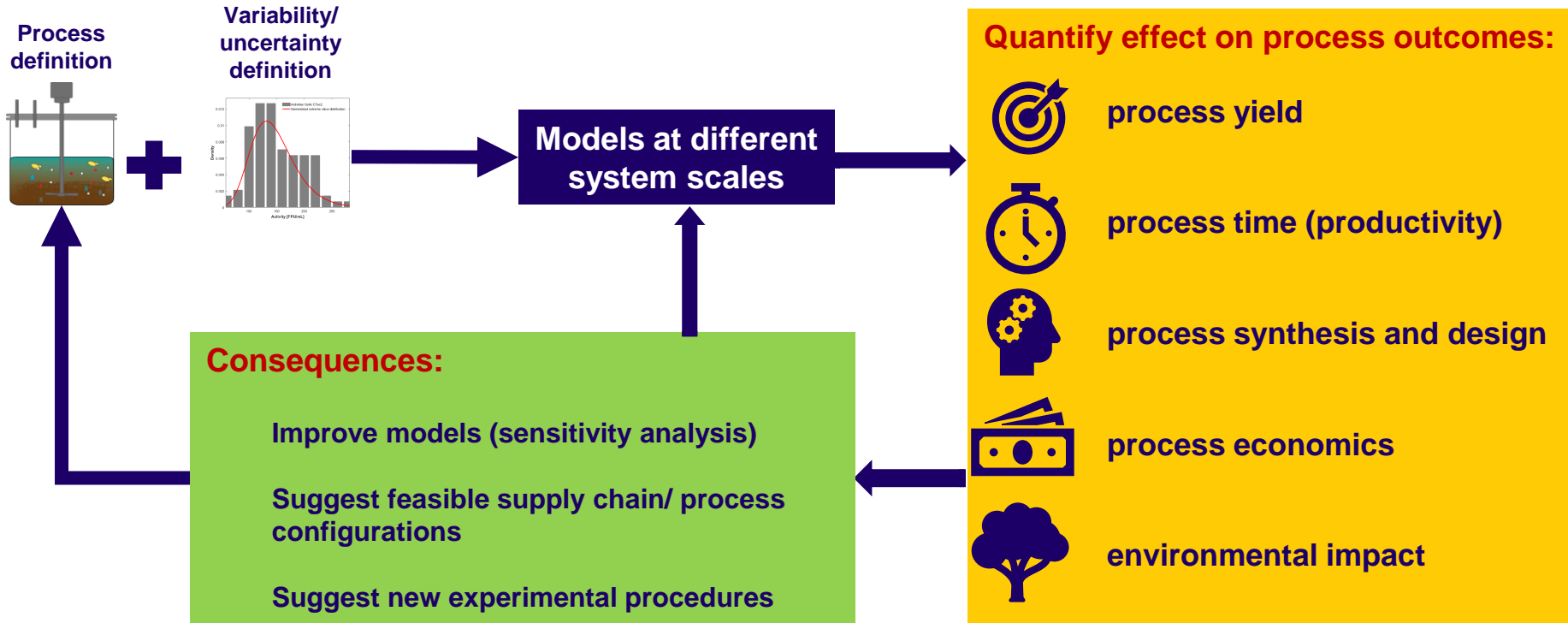
- 🎯 **High turbidity**
- 🎯 **Local viscosity differences**
- 🎯 **Solid compounds in liquid mixture**
- 🎯 **Complex chemical reaction system**

Effect of variability on process

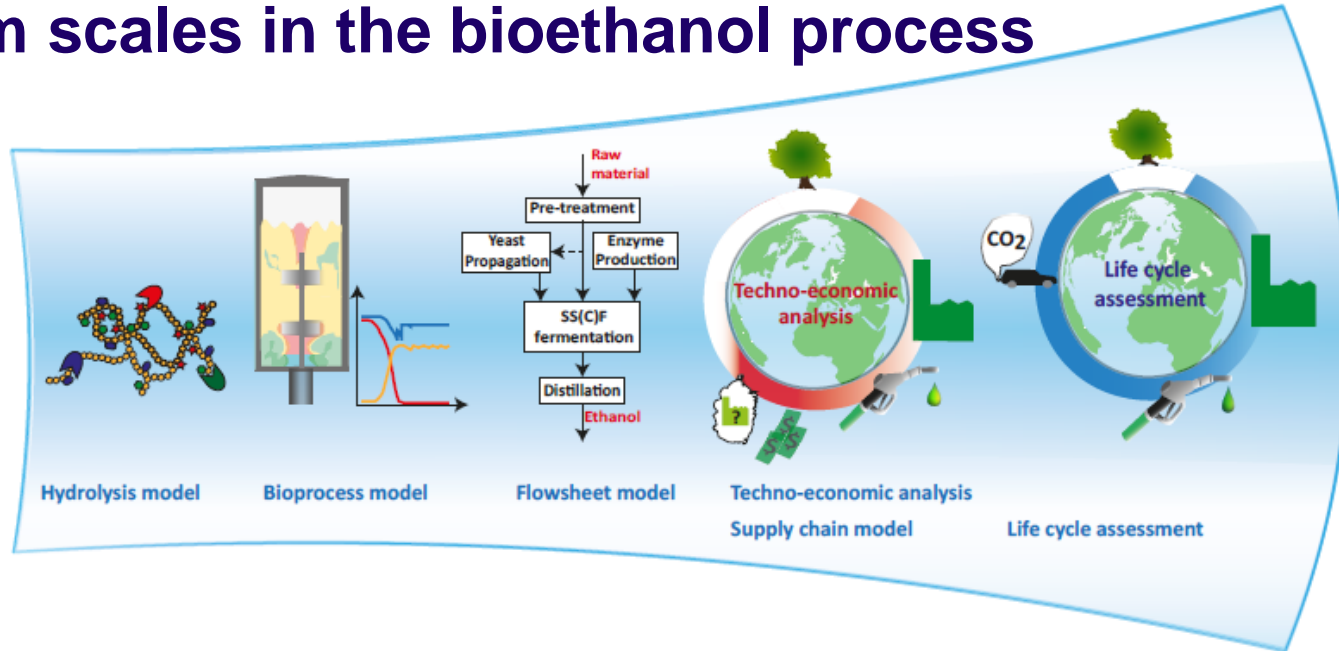


Integrate variability in process development at different scales!

Multi-scale uncertainty analysis – results & objectives

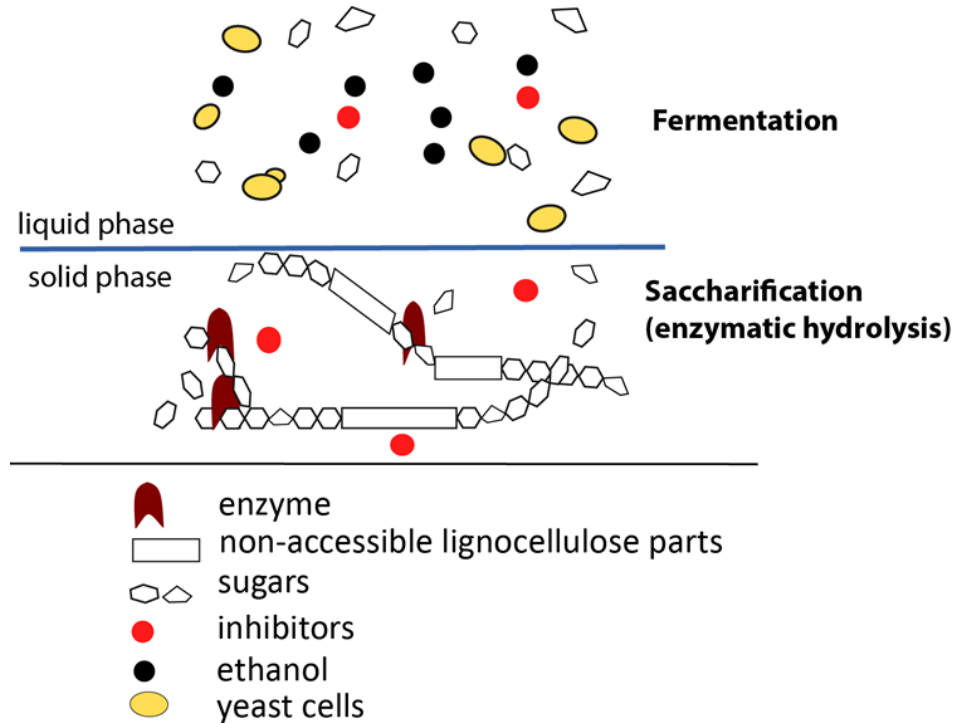


System scales in the bioethanol process



| Macro-molecular scale | Bioprocess scale | Factory scale | Global scale | Global scale |
|--|---|--------------------------------------|---|---|
| describe enzyme action | describe bioprocess | describe process integration | describe cost and profits | describe environmental impact |
| maximize hydrolysis yield develop enzyme cocktail | develop bioprocess perform optimal experimental designs perform optimal control | develop process synthesis and design | develop supply chain select economically best process alternative(s) | develop process based on environmental impact |

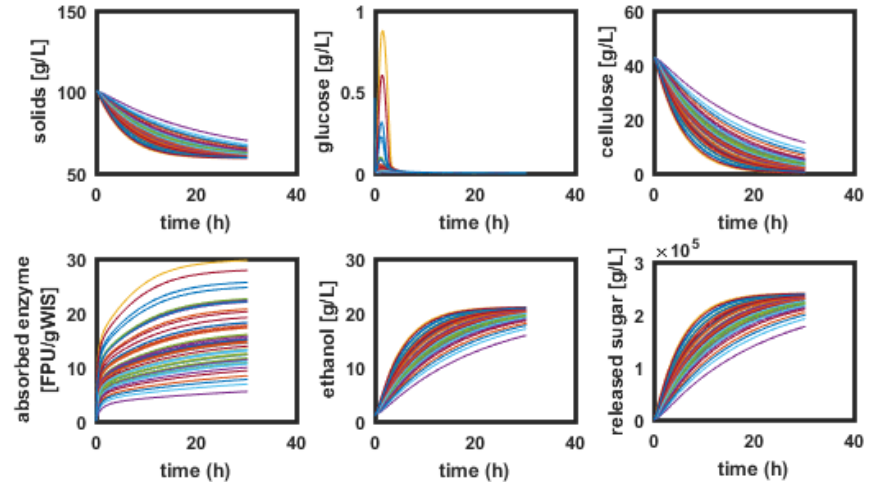
The bioprocess



The bioprocess/ hydrolysis model

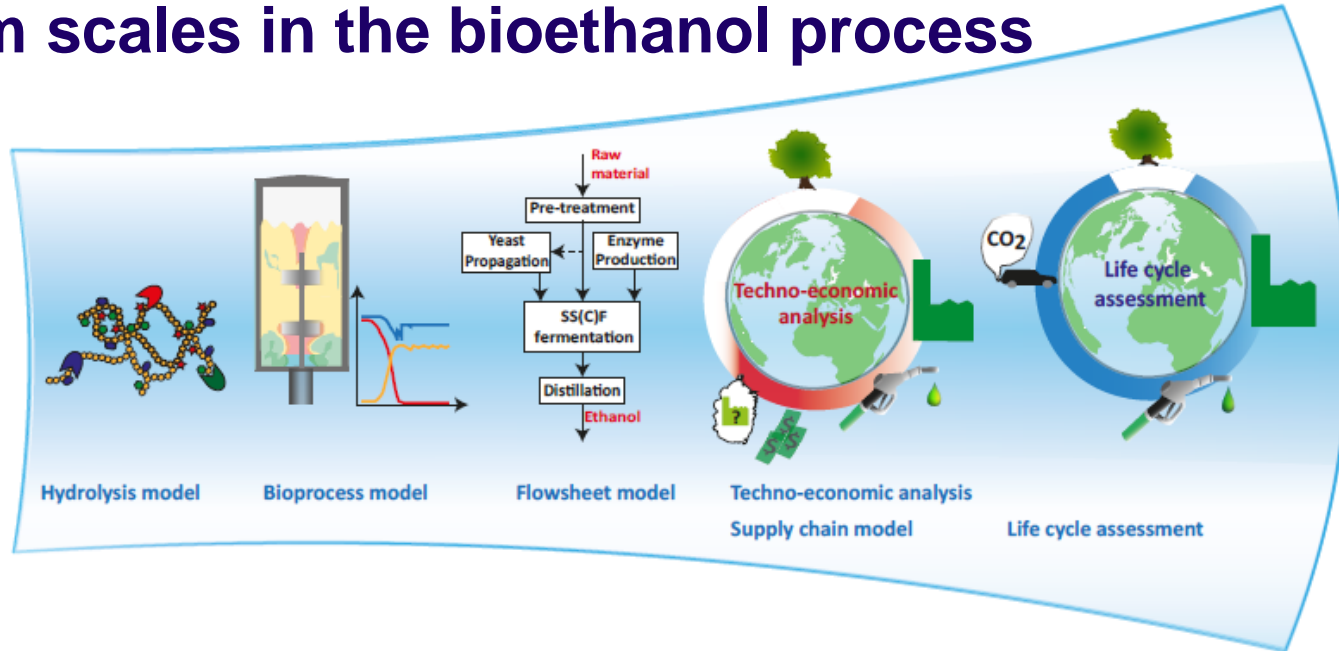
- Macro-kinetic model consisting of
 - 8 differential equations
 - 4 explicit algebraic equations

- Numerical solution in MATLAB using ode15s solver for stiff problems



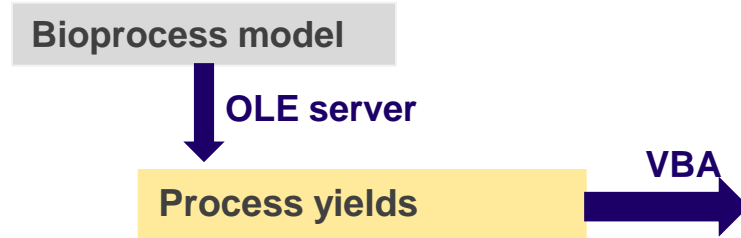
Simulation results for selected state variables for a batch process at demo plant (10m³) scale

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Flowsheet model and techno-economic analysis



SuperPro Designer

FERMENT-1 (Continuous Stoich. Fermentation) in P-33

Oper. Cond's | Volumes | Reactions | Vent/Emissions | Labor, etc. | Description

Reaction Data

Name: Hydrolysis cellulose Parallel ?

Reaction Limiting Comp.: Cellulose

Conversion Achieved: 74.00 %

Reaction Progress

Set Conversion: 93.00 %

Based on: Reaction Limiting Component

Ref. Comp.: Cellulose

Conversion Achieved: 74.00 %

Calculate to Achieve Target Concentration

[0.0000] [kg/m3] of [none]

Reaction Heat Ignore

Assume zero reaction heat at the enthalpy calculation reference temperature (0.0 °C).

Fermentation Mass Stoichiometry

162.16 Cellulose + 18.02 Water → 180.16 Glucose

Stoichiometry Balance for Hydrolysis cellulose

Reactants

| Component | Mass Coeff. |
|-------------|-------------|
| 1 Cellulose | 162.1600 |
| 2 Water | 18.0150 |

Total Mass: 180.175

Products

| Component | Mass Coeff. |
|-----------|-------------|
| 1 Glucose | 180.1570 |

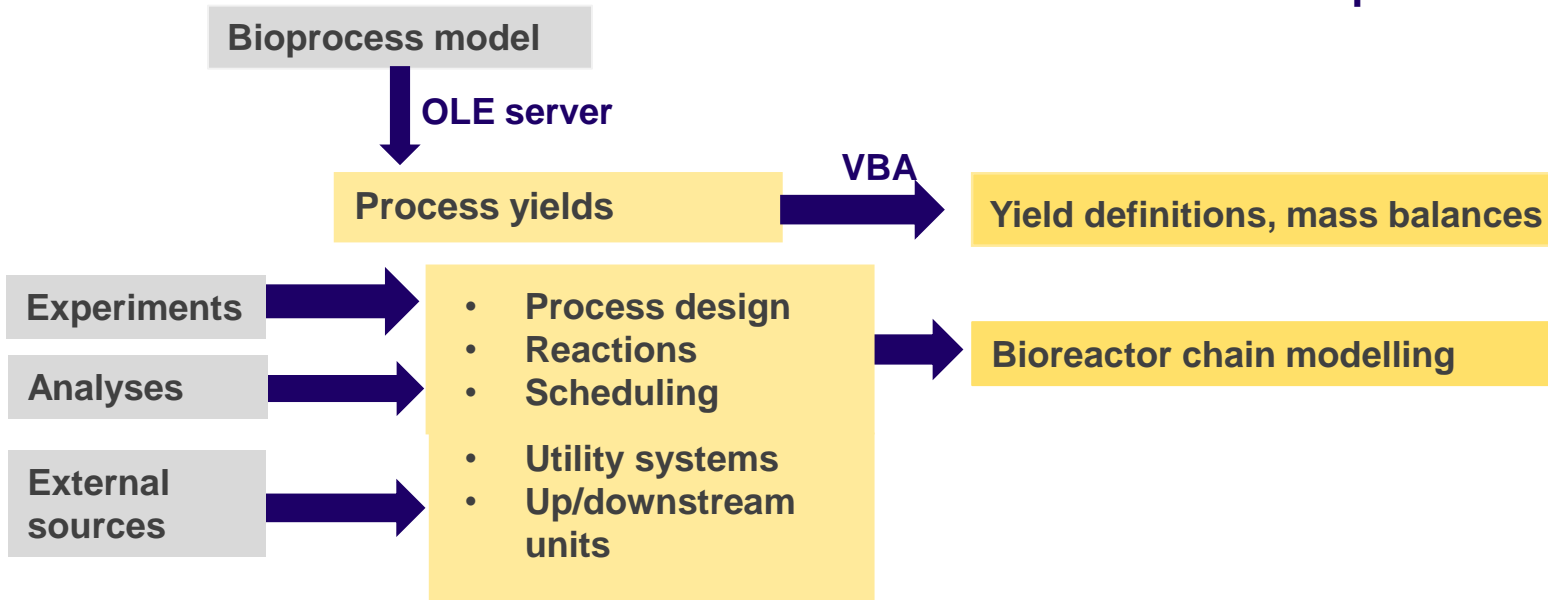
Total Mass: 180.157

Stoichiometric Coefficients: Mass Molar

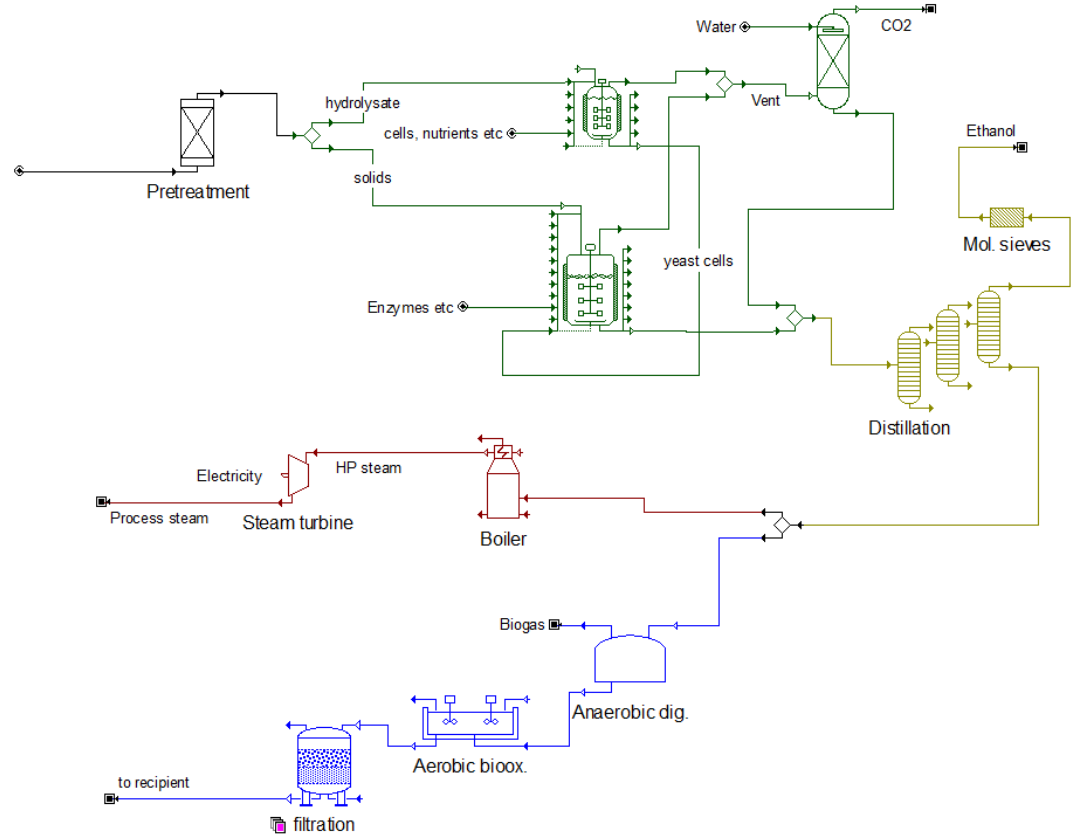
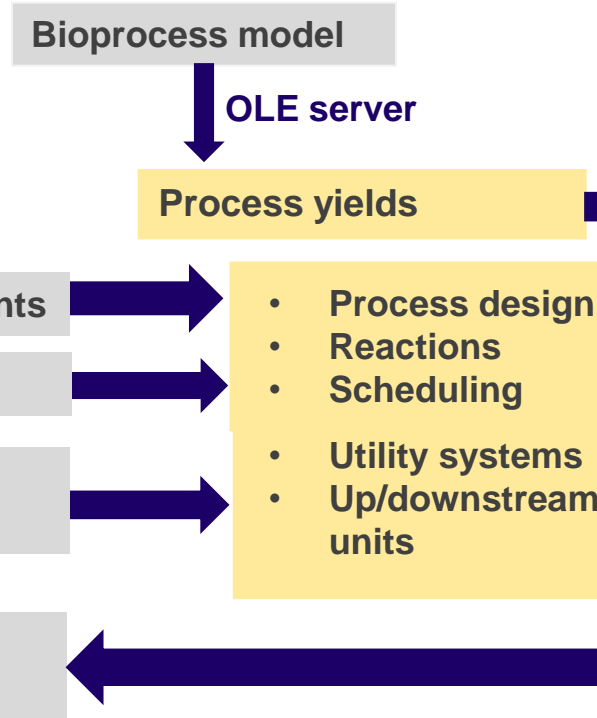
OK Cancel Help

Flowsheet model and techno-economic analysis

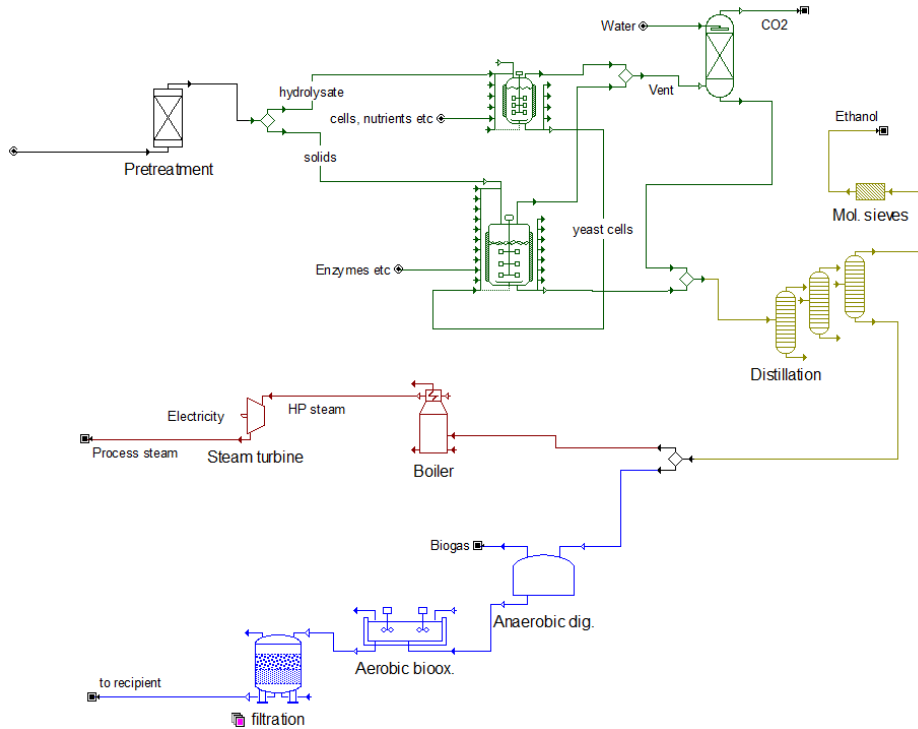
SuperPro Designer



Flowsheet model and techno-economic analysis



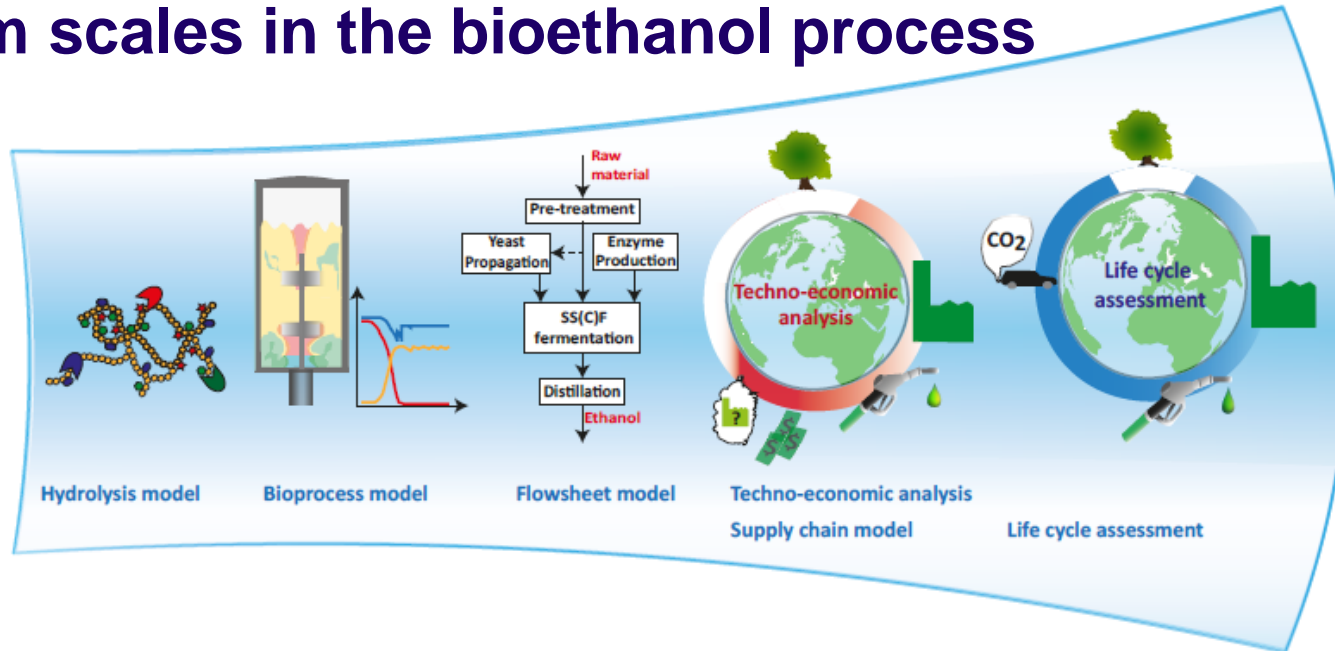
Flowsheet model– the outputs



mass/energy balances to:

- 🎯 **Techno-Economic Estimates**
- 🎯 **Supply chain analysis**
- 🎯 **Life cycle analysis**

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Life cycle assessment

- Calculates the potential environmental impact of ethanol production

- Inputs:

Database

Bioreactor model

Flowsheet model

- Software: openLCA

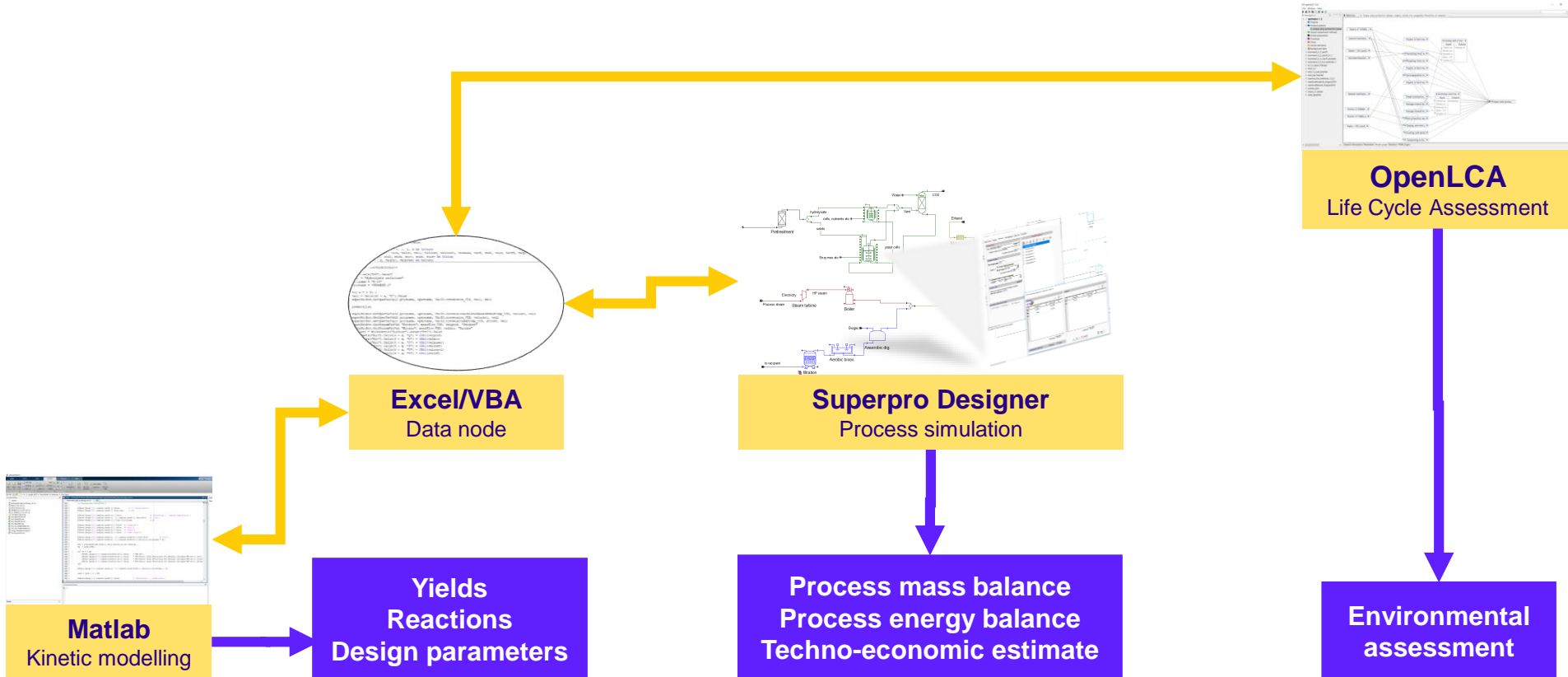
Contribution tree: Cellic CTec2, PEG, 30% DM, 7.5 FPU, PSSF

Flow: From shrub land, sclerophyllous - resource/land

Impact category: climate change - GWP 100a

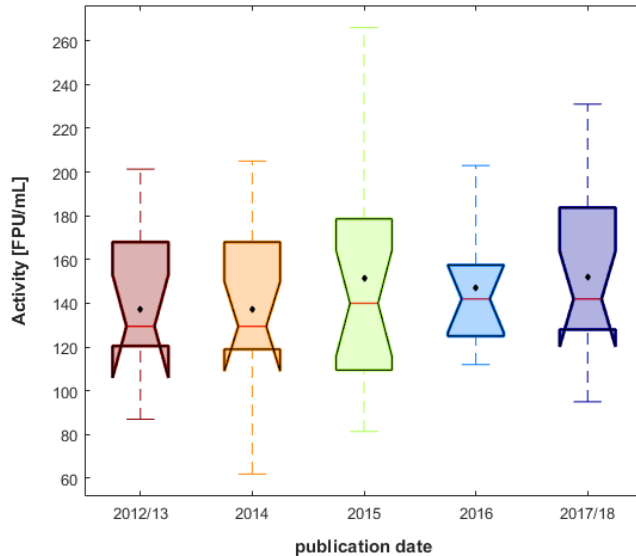
| Contribution | Process | Amount | Unit |
|--------------|---|---------|-----------|
| 100.00% | ethanol, product, PEG, Cellic CTec2, 30% DM, 7.5 FPU, PSSF | 2.56378 | kg CO2-Eq |
| 99.43% | ethanol, fermentation, PEG, Cellic CTec2, 30% DM, 7.5 FPU, PSSF | 2.54920 | kg CO2-Eq |
| 75.59% | enzyme, Cellic CTec2 - DK | 1.93798 | kg CO2-Eq |
| 20.26% | straw, pretreated - DK | 0.51942 | kg CO2-Eq |
| 19.43% | straw, prepared - DK | 0.49810 | kg CO2-Eq |
| 18.29% | wheat IP - CH | 0.46904 | kg CO2-Eq |
| 00.74% | transport, lorry >16t, fleet average - RER | 0.01902 | kg CO2-Eq |
| 00.39% | electricity mix - DK | 0.01004 | kg CO2-Eq |
| 00.83% | Combustion, dry wood residue, AP-42 (burning lignin) - RNA | 0.02132 | kg CO2-Eq |
| 02.02% | Polyethylene glycol | 0.05182 | kg CO2-Eq |
| 00.86% | sodium hydroxide, 50% in H2O, production mix, at plant - RER | 0.02205 | kg CO2-Eq |
| 00.70% | whey, to fermentation - CH | 0.01792 | kg CO2-Eq |
| 00.57% | Combustion, dry wood residue, AP-42 (burning lignin) - RNA | 0.01458 | kg CO2-Eq |

Data flow between scales

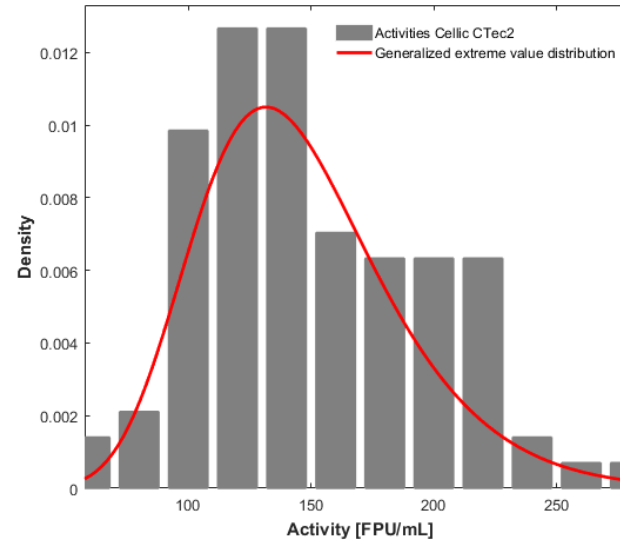


Variability in enzymatic activities – a case study

Step 1: Data collection



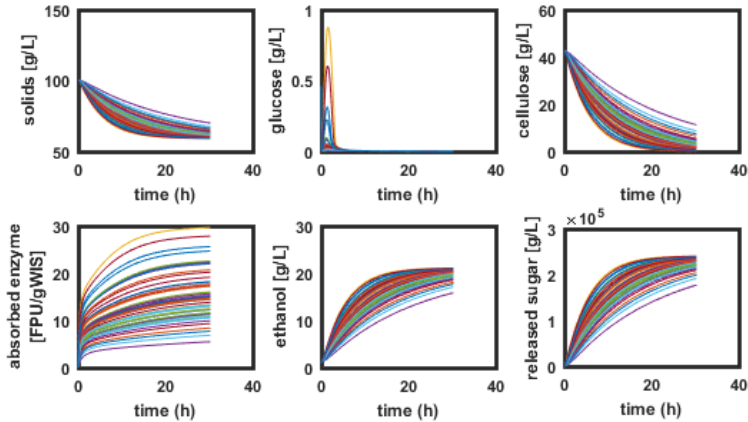
Step 2: Distribution fit



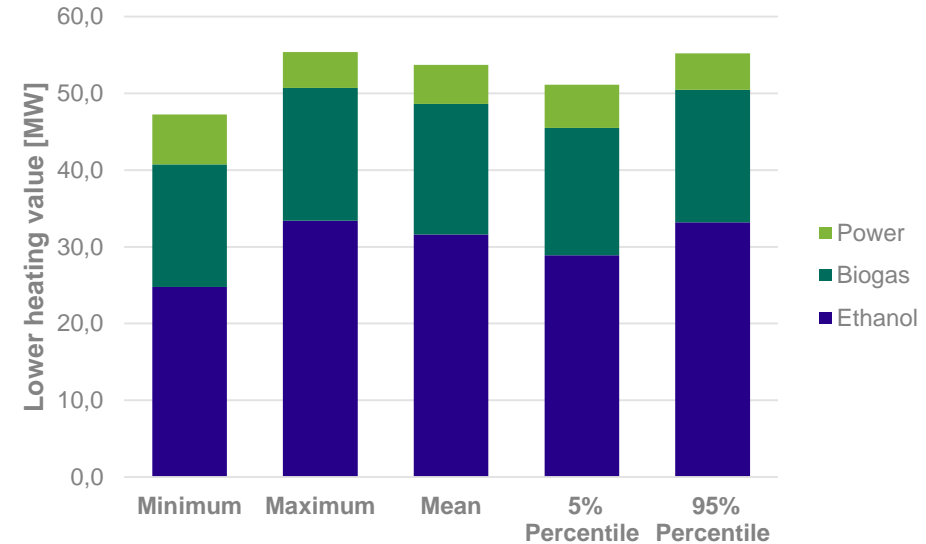
- Generalized extreme value distribution

Variability in enzymatic activities – a case study

Step 3: Propagation in bioprocess model



Step 4: Techno-economic assessment



The multi-scale concept:

- includes variability assessment in **early process development**
- allows to determine **stable process configurations**
- allows for **multi-objective optimization**
- shall allow to determine **optimal experimental conditions** to perform model validation experiments
- Ongoing: Include life cycle assessment in calculations



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